CORRECTIONS

page	line	should read
4	12 ↓	(at 1414°C)
23	Fig.1.2.8	interchange subscripts of α_L, α_S
37	end of §2.1.B	add: Let us also observe that the incompatibility of the initial and boundary data forces a discontinuity at the origin which the solution accomodates by an infinite initial speed of the interface.
38	equ.(25)	$\cdots 0 \le \zeta \le \Sigma(Fo)$, $Fo \ge 0$,
39	7 ↓	$\cdots$ material with rather high specific heat. In $\cdots$
39	9,10,11 ↓	$\cdots$ $T_m = 1996$ K $\cdots$ $\bar{c} = 1.12$ kJ/kg K $\cdots$ $L = 158$ kJ/kg. $\cdots$ $St = 12$.
41	12 ↓ , 3 ⇑	... affect the process ... $\cdots \alpha_L \cdots = 1.348 \times 10^{-3}$ $\cdots$
45	18 ↓	$c_S \approx 2\ J/g\,K$, $k_S \approx 0.023\ J/cm\,s\,K$, hence $\alpha_S = 0.0125\ cm^2/s$. You $\cdots$
47	Fig.2.2.1	interchange subscripts of α_L, α_S , delete vertical line and boundary condition at $x = l$
48	end of §2.2.A	add: As in the 1-phase case, we observe that the interface starts off with infinite speed, accomodating the discontinuity at the origin arising from the incompatible initial and boundary conditions.
54	9 ↓	$\hat{\tau} \ll \tau^*$, the melting curve at $\zeta^* = 0.2$ would change concavity but at a very early time.
57	2 ↓	$h'(x) = e^{x^2}\psi(x) > 0$ for $x > 0$.
62	below (3b), 14 ⇑	$\cdots -\rho_S c_S[T(X(t),t) - T_m] = \rho_L L$, $\cdots$ this term is expected to be
69	5 ⇑	$\cdots \rho_L L X' \cdots$
76	equ.(41),(42)	$\rho_L L X' + \frac{1}{2}\rho_L \cdots$ $\rho_S L X' - \frac{1}{2}\rho_S \cdots$
76	9 ↓	Note that in (40) and (42), $\cdots$
80	2 ⇑	$\cdots$ (**Figure 1.1.2**) $\cdots$
81	12 ↓	$\cdots$ see [CHADAM-RASMUSSEN, 1993] for $\cdots$
84	14 ⇑	$\cdots T_S \le T_m \cdots$
88	8 ⇑	$\cdots$ considerations. (delete "leading to (17) again")
88	6 ⇑	$\cdots$ to be $(1 - \rho_L / \rho_S)X_\infty$ or $(1 - \rho_S / \rho_L)X_\infty$ respectively, see $\cdots$
91	equ.(34)	$\frac{d}{dT}\Delta s = \left(\frac{\partial \Delta s}{\partial T}\right)_P + \left(\frac{\partial \Delta s}{\partial P}\right)_T \frac{dP}{dT} = \cdots$
95	equ.(53a),(53b)	$\cdots = T_m + g_S y + \cdots$ $\cdots = T_m + g_L y + \cdots$
95	2 ⇑	$\cdots = \cdots = -k_L \frac{\cdots}{\cdots}$
96	equ.(56) , 11 ⇑	$\Lambda(\omega) = \omega[\Gamma\omega^2(k_L + k_S) + \Gamma\omega V_0 \rho \Delta c + \cdots$ $\cdots$ delete the inequality : ($\omega^2 > \cdots$)
115	1 ↓	It can be $\cdots$ to give (delete "(PROBLEM 10)")
144	equ.(1a)	$\cdots = k_L \cdots$
153	3 ⇑ , 2 ⇑ , 1 ⇑	constant speed of $10\ cm/s$ $\cdots$ $\cdots$ [use $\nu = 0.01$ $\cdots$ $\cdots$ 18 minutes $\cdots$
155	equ.(3b)	$\cdots$, $\cdots$, $\Sigma(\tau) = X(t) / \hat{x}$
160	2 ⇑	delete "$c = c_L / c_S$"
161	equ.(28c)	replace $\varepsilon\delta c$ by $\varepsilon(k-1)$
166	equ.(15)	denominator: $5 + 2\boldsymbol{St}_L + \cdots$
166	Table 3.4.2	replace top five entries of last two columns by
		0.107E-06 0.107E-06
		-0.624E-07 -0.680E-07
		0.109E-06 -0.678E-07
		0.191E-05 -0.368E-05
		0.576E-04 -0.116E-03
169	equ.(4b)	in the denominator, replace upper case "L" by lower case "l"
177	12 ↓	$\cdots$ (PROB.14)
189	10 ↓	$\cdots$ **§4.1.G**).
193	15 ↓	**local truncation error:** $\cdots$ **$[u(x_j, t_n)]$**
200	equ.(52)	$E_{ijk}^{n+1} = \cdots$
208	19 ⇑ , 8 ⇑ , 7 ⇑	$\cdots$ $T(x,t) = \exp(-\pi^2 \alpha t / l^2) \cdot 100 \cos(\pi x / l)$, $\cdots$ repeating (b) $\cdots$ $\cdots$ from (b).
220-2		in captions of Fig.4.3.1(a),(b), Fig.4.3.4(a),(b): replace $x = .3$ by $x = 0.2$
224	equ.(24)	numerator of first fraction: $u_{j-1}^{n+1} - u_j^{n+1}$
225	6 ↓	$(E - \rho L) / \rho c_L$, $\rho L \le E$ (liquid).
239	13 ⇑, 7 ⇑	$\cdots$ At some point either $\cdots$ $\cdots$ a slab $-l_w \le x \le l$ $\cdots$
254	2 ↓	$\cdots - H\phi_t - div(\phi \nabla u) + \cdots$
255	10 ⇑	$N_t^\Sigma = \cdots$, and $\vec{N}_x^\Sigma = \cdots$
305		ALEXIADES, V. and J.B. DRAKE, " $\cdots$ " in *Free boundary problems involving solids,* $\cdots$ (1993).
307		CHADAM, J.M. and H. RASMUSSEN, "*Free boundary problems involving solids,*" $\cdots$ (1993).